

IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for removing trialkylammonium formate from methylolalkanes obtained by condensation of formaldehyde with a higher aldehyde, comprising

decomposing the trialkylammonium formate at elevated temperature, in the presence of a hydrogen-containing gas, over a catalyst comprising ruthenium supported on titanium dioxide, wherein the catalyst is obtained by impregnating ruthenium in the titanium dioxide support, and wherein said catalysts have a pore volume of from 0.1 to 1m/g and a BET surface area of from 5 to 500 m²/g.

Claim 2 (Previously Presented): The process of claim 1, wherein the catalyst ~~has~~ comprises a ruthenium content of from 0.1 to 10% by weight.

Claim 3 (Previously Presented): The process of claim 1, wherein the titanium dioxide comprises shaped titanium dioxide bodies obtained by treatment of commercial titanium dioxide, before or after shaping, with from 0.1 to 30% by weight of an acid in which titanium dioxide is sparingly soluble.

Claim 4 (Previously Presented): The process of claim 1, carried out at a temperature of from 100 to 250°C.

Claim 5 (Previously Presented): The process of claim 1, carried out at a pressure of from 1×10^6 to 15×10^6 Pa.

Claim 6 (Previously Presented): The process of claim 1, carried out in a hydrogenation reactor.

Claim 7 (Original): A catalyst comprising ruthenium supported on shaped titanium dioxide bodies, wherein the shaped titanium dioxide bodies are obtained by treatment of commercial titanium dioxide, before or after shaping, with from 0.1 to 30% by weight of an acid in which titanium dioxide is sparingly soluble.

Claim 8 (Previously Presented): The process of claim 2, wherein the titanium dioxide comprises shaped titanium dioxide bodies obtained by treatment of commercial titanium dioxide, before or after shaping, with from 0.1 to 30% by weight of an acid in which titanium dioxide is sparingly soluble.

Claim 9 (Previously Presented): The process of claim 2, carried out at a temperature of from 100 to 250°C.

Claim 10 (Previously Presented): The process of claim 3, carried out at a temperature of from 100 to 250°C.

Claim 11 (Previously Presented): The process of claim 2, carried out at a pressure of from 1×10^6 to 15×10^6 Pa.

Claim 12 (Previously Presented): The process of claim 3, carried out at a pressure of from 1×10^6 to 15×10^6 Pa.

Claim 13 (Previously Presented): The process of claim 4, carried out at a pressure of from 1×10^6 to 15×10^6 Pa.

Claim 14 (Previously Presented): The process of claim 2, carried out in a hydrogenation reactor.

Claim 15 (Previously Presented): The process of claim 3, carried out in a hydrogenation reactor.

Claim 16 (Previously Presented): The process of claim 4, carried out in a hydrogenation reactor.

Claim 17 (Previously Presented): The process of claim 5, carried out in a hydrogenation reactor.

Claim 18 (Previously Presented): The process of claim 1, carried out at a temperature of from 120 to 180°C.

Claim 19 (Previously Presented): The process of claim 2, carried out at a temperature of from 120 to 180°C.

Claim 20 (Previously Presented): The process of claim 3, carried out at a temperature of from 120 to 180°C.